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CPCE key process steps in post-combustion carbon utilization

The most poignant process sections of CPCE for the upgrading of existing fossil energy plants

- 1. Execution of Advanced Combustion in the gas turbine and fossil fuel fired power plants to obtain a high concentrated CO₂-rich gas stream without nitrogen, at low gas flow rate, factually <u>zero-Dollar value feedstock</u>
- 2. Waste heat recovery with factually as <u>zero-Dollar value energy</u> via First Bairamijamal Thermodynamic Cycle that backs up the electrolysis eventually via <u>DC Supply Line#1</u>
- 3. Harnessing the useless waste heat to useful electric AC electricity and/or process power integrated in the First Bairamijamal Cycle and HR sections for syngas and oxygen downstream of an auxiliary gas turbine, which supplies AC current, then eventually via <u>DC Supply Line#2</u>
- 4. Use of process power thereof for the cooling and separation of CO₂ from that CO₂-rich CO₂-Stream, obtaining liquid carbon dioxide at high mass flow rate for the electrochemical conversion with water to syngas and oxygen at high yield
- 5. Use of that generated AC power under (2) and (3) for the DC back-up power hence referred to <u>DC Supply line #1 &2</u> for the electrochemical conversion of the obtained liquid carbon dioxide for the production of anodic oxygen and cathodic syngas in the CPCE's HPLTE-SG (High Pressure Low Temperature Electrochemical Syngas Generator)
- 6. Harnessing the high pressure low temperature gaseous products of the electrolysis for heat recovery and to the "closing trajectory" of the First Bairamijamal Cycle under (2) for generation of additional DC power by use of multi-stage oxygen and multi-stage syngas turbines, which provides back-up AC electric power for running the electrolysis under (5) i.e. via <u>DC Supply Line #3</u> and the <u>DC Supply Line #4</u>
- 7. Utilization of the most portion of the anodic oxygen for the Advanced Combustion by way of flue gas recirculation and flue gas oxyfueling under (1) and (3)
- 8. Conversion of a little portion of the syngas with steam via water shift converter to hydrogen and CO₂, whereas this CO₂ is recycled for re-use back to the process in (4)
- 9. Harnessing that portion of hydrogen with little portion of anodic oxygen to generate the remaining need for the DC current by use of fuel cell, i.e. <u>DC Supply Line #5</u> under (5)
- 10. Delivery of syngas to an adjacent plant for high value final products like jet fuel, transportation gasoline, ethanol, methanol, and great number of other chemicals (vide attached chart) that accomplishes the lowest ever costs for production i.e. a return of investment of less than two years
- 11. Dispatch of pure oxygen to the market and excess AC power to the grid from the First Bairamijamal Cycle.